Title
Efficiency of electrochemical systems

Permalink
https://escholarship.org/uc/item/58m609bn

Journal
Journal of Power Sources, 134(2)

ISSN
0378-7753

Authors
Rao, A
Maclay, J
Samuelsen, S

Publication Date
2004-08-01

DOI
10.1016/j.jpowsour.2004.02.028

License
CC BY 4.0

Peer reviewed
Short communication
Efficiency of electrochemical systems
Ashok Rao*, James Maclay, Scott Samuelsen
Advanced Power and Energy Program, University of California, Irvine, CA 92697-1550, USA
Received 9 February 2004; accepted 22 February 2004
Available online 10 June 2004
Abstract
The second-law efficiency is proposed for measuring and comparing the performance of electrochemical processes. It measures how close the process approaches a reversible process. Other definitions of efficiency found in the literature based on the first law of thermodynamics can generate efficiency values that are >100% for certain systems depending on whether the change in entropy for the overall chemical reaction involved in the process is positive or negative. Such efficiency values are misleading while making it difficult to compare processes that absorb or release significant quantities of thermal energy. Use of the proposed efficiency which is within the framework of the second law of thermodynamics, can reach 100% only in the limit of a reversible process and will always stay <100% whether the entropy change is positive or negative. Furthermore, it accounts for the quality of thermal energy added to or removed from the system and thus provides a more consistent way of comparing different types of electrochemical devices. This consistency will allow better comparison of performance on a widespread basis, i.e., between groups working on distinct electrochemical systems.
© 2004 Elsevier B.V. All rights reserved.
Keywords: Fuel cells; Electrolyzers; Efficiency; Thermodynamics

1. Introduction
The performance of an electrochemical device such as a fuel cell when measured in terms of the thermal efficiency or the "first-law efficiency" of the system can be quite misleading. Expressing the performance in terms of the thermal efficiency does not provide a true yardstick to measure the inefficiencies within the system since not all of the energy released by reaction within the cell may be converted to useful work without violating the second law of thermodynamics. Furthermore, as pointed out by [1], the thermal efficiency of a fuel cell can be >100% in cases where the entropy change for the overall reaction occurring within the cell is positive. This can be seen from the following.
The expression for the thermal efficiency (ηFC) of a fuel cell is defined by the expression:

\[ η_{FC} = \frac{W_{out}}{-ΔH_R} \]  

where \( W_{out} \) is the useful work produced by the process, and \( ΔH_R \) is the enthalpy change for the reaction. From the first law of thermodynamics:

\[ η_{FC} = \frac{ΔH_R - Q_a}{-ΔH_R} \]  

where \( Q_a \) is the heat added to the system. For a reversible fuel cell operating isothermally at a temperature \( T \), the thermal efficiency then becomes

\[ η_{FC} = \frac{ΔH_R + TΔS_R}{-ΔH_R} \]  

\[ = \frac{ΔG_R}{-ΔH_R} \]  

where \( ΔS_R \) is the entropy change and \( ΔG_R \) is the Gibbs free energy change (represents the maximum useful work that may be produced) for the reaction. As can be seen from Eq. (3) above, for a reaction that releases energy where \( ΔH_R \) is negative, efficiencies >100% can be calculated when \( ΔS_R \) is positive.

To circumvent this problem of calculating efficiencies >100% while comparing the thermodynamic performance of fuel cells with heat engines, two separate definitions for the thermal efficiency of a fuel cell depending on whether \( ΔS_R \) is positive or negative have been suggested [2]. In cases where \( ΔS_R \) is negative, the above expression is utilized while when \( ΔS_R \) is positive, \( η_{FC} \) is always reduced to 100% by replacing the denominator in the above expression.
with \( -\Delta H_k + T \Delta S_k \) or \( -\Delta G_k \). This methodology, however, leads to an inconsistent set of yardsticks when comparing the performance of different types of fuels in a fuel cell. Next, in the case of an electrolyzer, an energy efficiency (\( \eta_{el} \)) has been defined [3] by the ratio of the thermoneutral cell voltage (\( U_{\text{TN}} = \Delta H_k/zF \)) and the actual cell voltage (\( U_{\text{act}} \)):

\[
\eta_{el} = \frac{U_{\text{TN}}}{U_{\text{act}}} = \frac{\Delta H_k}{T \Delta S_k + zF U_{\text{TN}}} \tag{5}
\]

where \( z \) is the number of electrons transferred per reaction, and \( F \) is the Faraday constant. The above expression may also be written as

\[
\eta_{el} = \frac{\Delta H_k}{\Delta G_k + zF U_{\text{TN}}} \tag{6}
\]

where \( U_{\text{TN}} \) is the cell overvoltage, and \( \Delta H_k, \Delta G_k \) and \( \Delta S_k \) are the changes in enthalpy, Gibbs free energy and entropy for the decomposition reaction, i.e., the reaction proceeding in the opposite direction of that in a fuel cell when, e.g., a water electrolyzer and a H2 based fuel cell are proceeding in the opposite direction of that in a fuel cell (in the case of an electrochemical process) while exergy of \( \frac{\Delta H_k}{T \Delta S_k} \). The above expression for the second-law efficiency measures how close the process approaches a reversible process. This efficiency definition which is within the frame work of the second-law can reach 100% only in the limit of a reversible process and will always stay <100% whether the entropy change for the reaction is positive or negative. It also provides a true measure of how much of a gain in performance can be realized by making improvements to the process or device. Furthermore, it accounts for the quality of thermal energy added to or removed from the system and thus provides a more consistent way of comparing different types of electrochemical devices. The second-law efficiency comparison also provides a standard methodology, which if universally adopted may provide a consistency that may be presently lacking in the fuel cell/electrolyzer community. This consistency could allow better comparison of performance on a widespread basis, i.e., between groups working on distinct electrochemical systems.

2. The second-law efficiency

In order to overcome the limitations discussed in the preceding, it is proposed that the "second-law efficiency" [4] be utilized for measuring or comparing the performance of such electrochemical devices or processes; the general form defined as

\[
\eta = \frac{\sum \chi_{\text{out}} + \sum Q_{\text{out}}(1 - T_0/T_{\text{out}}) + W_{\text{out}}}{\sum \chi_{\text{in}} + \sum Q_{\text{in}}(1 - T_0/T_{\text{in}}) + W_{\text{in}}} \tag{9}
\]

where \( \eta \) is the second-law efficiency, \( \sum \chi_{\text{out}} \) and \( \sum \chi_{\text{in}} \) are the sum of the exergies of the streams leaving and entering the system, respectively, \( T_{\text{in}} \) is the temperature at which heat \( Q_{\text{in}} \) is added to the system, \( T_{\text{out}} \) is the temperature at which heat \( Q_{\text{out}} \) is removed from the system, \( T_0 \) is the temperature of the surroundings (in practical applications, would be the mean temperature at which heat may be rejected to the surroundings such as cooling water). The second terms in the numerator and the denominator of Eq. (9) express the Carnot cycle efficiency of converting the heat to work. \( W_{\text{out}} \) and \( W_{\text{in}} \) are the useful work developed by the system and that expended on the system, respectively (e.g., electrical in the case of an electrochemical process) while exergy of a stream is the maximum work producing capability of the stream as it is equilibrated with the surroundings.

The above expression for the second-law efficiency measures how close the process approaches a reversible process. When the kinetic and potential energy effects may be neglected, exergy (\( \chi \)) for a stream is defined as [5]:

\[
\chi = W_{\text{sensible}} + W_{\text{expansion}} + W_{\text{concentration}} + W_{\text{chemical}} \tag{10}
\]

where \( W_{\text{sensible}} \) is the reversible work that may be obtained by a heat engine taking heat from the stream (at temperature \( T \)) and rejecting heat to the environment (at temperature \( T_0 \)). \( W_{\text{expansion}} \) is the irreversible work that may be obtained from the stream at pressure \( P \) by isothermal expansion (after conversion of the sensible energy to the pressure of the environment (\( P_0 \)). \( W_{\text{concentration}} \) is the additional work that may be obtained by reversibly diffusing a noncombustible component \( i \) within the stream at partial pressure \( P_i \) through a membrane to the environment where it may be at a partial pressure of \( P_{i0} \), and \( W_{\text{chemical}} \) is the work (after cooling and expansion) that may be produced by oxidation of the combustibles that may be present in the stream with enough excess air such that the partial pressure of the \( CO_2 \) corresponds to that in the ambient. Thus,

\[
\chi = - \int \left( 1 - \frac{T_0}{T} \right) C_P dT + \int R T \left( \ln \frac{P}{P_0} + \sum \ln \frac{P_i}{P_{i0}} \right) - \Delta G_{\text{reaction}} \tag{11}
\]

where the integral in the first term on the left-hand side of Eq. (11) is evaluated from the initial to the final temperature of the stream, \( C_P \) is the specific heat of the stream, \( \Delta G_{\text{reaction}} \) is the Gibbs free energy change for the oxidation reaction of the combustibles at the temperature of the environment.

The first term on the left-hand side of Eq. (11) defines the maximum work that may be obtained based on the Carnot
cycle efficiency. This term as defined in [5] is modified to include the work potential of streams that contain water in the form of vapor which could undergo a phase change when equilibrated with the environment. This term ($W_{\text{heat}}$) is defined as

$$W_{\text{heat}} = -\int \left(1 - \frac{T_0}{T}\right) dH$$

(12)

where $H$ is the enthalpy which may include both sensible as well as latent heats.

The second term of Eq. (11) is modified in order to be able to handle streams that contain water as a vapor or as a liquid and may undergo phase change:

$$W_{\text{expansion}} = -\Delta G_{\text{expansion}}$$

(13)

where $\Delta G_{\text{expansion}}$ is the Gibbs free energy change of the stream as its pressure is reduced to that of the environment.

The proposed next step in the path for the stream to equilibrate with the environment is the reversible isothermal oxidation reaction at $T_0$ of the combustibles present in the stream utilizing the ambient air:

$$W_{\text{chemical}} = -\Delta G_{\text{chemical}}$$

(14)

The proposed final step in the path for the stream to equilibrate with the environment is the reversible isothermal expansion at $T_0$ of component $i$ through the hypothetical reversible membrane to its partial pressure in the ambient air (i.e., as depicted in Fig. 1 by allowing the component to reversibly exchange through a selective membrane between the stream and a chamber, and similarly between the ambient air and a second chamber, the two chambers being connected by a turbo-expander operating reversibly between the two pressures):

$$W_{\text{concentration}} = -\Delta G_{\text{concentration}}$$

(15)

This work potential would be typically small with most current practical fuel cell systems, unless $O_2$ is used instead of air as the oxidant in which case it would allow accounting for the work required to separate $O_2$ from air. Similarly, in the case of a water electrolyzer, if $O_2$ is produced as a byproduct for sale, credit may be given to this stream.

The other components considered for this type of work potential would be water vapor and carbon dioxide produced from the oxidation of the fuel or those present in the exhaust in the case of a fuel cell, although their contribution to the overall exergy may be quite small. The oxygen and nitrogen present in the exhaust of a fuel cell could also produce work by expansion but in the reverse direction, since a concentration gradient may exist for these components between the system and the environment (the concentration in the environment being typically higher). Such considerations would however provide impractical guidance for system improvements.

4. Simplified expression for efficiency

In many practical applications, the total exergy of the streams entering in the case of a fuel cell or leaving in the case of a water electrolyzer is predominantly due to the chemical energy contained in the stream. Furthermore if both $Q_{in}$ and $Q_{out}$ are small or if $T_{in}$ tends to be near ambient temperatures and the thermal energy in the exhaust cannot be utilized for generating additional power, the expression for the second-law efficiency reduces to the following expressions:

For a fuel cell operating near ambient temperature:

$$\eta_{II} = \frac{W_{\text{out}}}{\Delta G_{R}}$$

(16)

since $-\Delta G_{R} \sim \sum \chi_{in}$ for the oxidation reaction of the fuel, $\Delta G_{R}$ being the Gibbs free energy change for the reaction representing the maximum work that may be produced by the overall chemical reaction.

Or,

$$\eta_{II} = \frac{U_{\text{ACT}}}{U_{\text{REV}}}$$

(17)

For an electrolyzer operating near ambient temperature:

$$\eta_{II} = \frac{-\Delta G_{R}}{W_{m}}$$

(18)

since $-\Delta G_{R} \sim \sum \chi_{out}$ for the oxidation reaction of the product, e.g., $H_2$ in the case of a water electrolyzer, and $\Delta G_{R}$ being the Gibbs free energy change for the oxidation of the product representing the maximum work that may be produced by the overall chemical reaction.

Or,

$$\eta_{II} = \frac{-\Delta G_{R}}{W_{m}}$$

(19)

$$= \frac{U_{\text{REV}}}{U_{\text{ACT}}}$$

(20)

<table>
<thead>
<tr>
<th>System</th>
<th>Stream</th>
<th>Chamber 1</th>
<th>Chamber 2</th>
<th>Environment</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td>Pure Component $i$ at Partial Pressure $P_i$</td>
<td>Pure Component $i$ at Total Pressure $P_i$ in Equilibrium with System</td>
<td>Reversible Expander</td>
<td>Pure Component $i$ at Total Pressure $P_i$ in Equilibrium with Environment</td>
</tr>
</tbody>
</table>

Fig. 1. Reversible expansion of component after diffusion through membrane.
where $U_{\text{REV}}$ is the reversible cell voltage required by the electrolyzer.

5. Conclusions/recommendations

The second-law efficiency for measuring and comparing the performance of electrochemical processes measures how close the process approaches a reversible process. It provides a true yardstick to measure the inefficiencies within the system. Furthermore, it accounts for the quality of thermal energy added to or removed from the system and thus provides a more consistent way of comparing different types of electrochemical devices. This consistency may allow better comparison of performance on a widespread basis, i.e., between groups working on distinct electrochemical systems. Other definitions of efficiency found in literature based on the first law of thermodynamics can generate efficiency values that are >100% for certain systems depending on whether the change in entropy for the overall chemical reaction involved in the process is positive or negative. Such efficiency values are misleading while making it difficult to compare processes that absorb or release significant quantities of thermal energy. The proposed use of the second-law efficiency which is within the frame work of the second law of thermodynamics, can reach 100% only in the limit of a reversible process and will always stay <100% whether the entropy change is positive or negative.

References